





# Polymer adsorption isotherms with *NaCl* and *CaCl*<sub>2</sub> on kaolinite substrates

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#### Abstract

During polymer injection in enhanced oil recovery processes, polymeric molecules are attached to the rock surface as a result of a series of interactions between both components, leading to concentration decrease on the injected batch. This phenomenon, known as adsorption [18], can be estimated by analytical models and depends on several factors like the type of rock, degree of hydrolysis and polymer concentration, reservoir temperature, salinity of formation water, among other aspects. This paper shows the results of 144 statics tests where salinity (*NaCl* and *CaCl*<sub>2</sub>) and polymer concentration were taken as the parameters to be changed in order to determine which analytical model is the most accurate for the prediction of experimental results. The abnormal adsorption tendency with *NaCl*, indicates that the grater salinity value, the lesser adsorption value concentrations. This is mainly due to the response of the kaolinite substrate to flocculation.

Keywords: enhanced oil recovery; polymer injection; analytical models; adsorption; flocculation.

# Isotermas de adsorción de polímeros con *NaCl* y *CaCl*<sub>2</sub> en sustratos de caolinita

#### Resumen

Durante la inyección de polímeros en procesos de recobro mejorado de petróleo, las moléculas poliméricas son atraídas a la superficie de la roca como resultado de una serie de interacciones entre ambos componentes, llevando finalmente a una disminución en la concentración del bache inyectado. Este fenómeno, conocido como adsorción [18], depende del tipo de roca, grado de hidrólisis y concentración del polímero, temperatura del yacimiento, salinidad del agua de formación, entre otros, y puede ser estimado a partir de modelos analíticos. Este trabajo muestra los resultados de 144 pruebas estáticas, en donde la salinidad (*NaCl* y *CaCl*<sub>2</sub>) y la concentración de polímero se tomaron como parámetros a variar, con el fin de determinar cuál de los modelos analíticos es capaz de predecir en una forma más acertada los resultados experimentales. Finalmente se discute la tendencia anormal de la adsorción en presencia de *NaCl*, donde mayores valores de salinidad resultaron en menores valores de adsorción, como respuesta principalmente a la floculación de la caolinita.

Palabras clave: recobro mejorado; inyección de polímeros; modelos analíticos; adsorción; floculación.

#### 1. Introduction

Decrease of light crude oil around the world has posed a great challenge for the petroleum industry; one of the alternatives to extract a greater amount of remnant oil in this type of mature reservoirs is the implementation of an Enhanced Oil Recovery method like polymer injection. This technique represents an improvement when compared to conventional water injection because the viscosity of the displacing fluid is increased in order to decrease the oil mobility ratio in the reservoir [1,3,6,7,12,16,33-35].

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However, during the passage through the porous media, the polymeric molecules are attracted by the rock surface as a result of physical and chemical interactions between the components [2,4,6-9,12,16,20,22,28,34]. This phenomenon, known as adsorption, decreases polymer concentration in the injected solution and, therefore, the efficiency of the process is seriously affected.

Adsorption effects can be studied in the laboratory by the conduction of both static and dynamic testing. Static testing determines adsorption for a given substrate and it is sometimes overestimated when compared to what occurs at reservoir level as a result of the analysis of a greater surface area than the real one. However, this technique is an economic option to determine adsorption behavior based on the variation of a specific parameter: salinity.

In this research paper, an isotherm series were built from 144 static tests on kaolinite substrate, changing the polymer concentration (one commercial HPAM) and brine salinity in order to determine the effect of Sodium Chloride (NaCl) and Calcium Chloride ( $CaCl_2$ ) on adsorption. Then, the experimental data produced were adjusted to the Henry, Langmuir and Freundlich adsorption isotherm; the corresponding variation is determined considering the various scenarios. Finally, the reasons for an unusual decrease of adsorption when NaCl concentration increases are discussed as a result of a marked flocculation of the kaolinite substrate.

## 2. Methodology

Polymer adsorption in petroleum reservoirs depends on various parameters such as the type of polymer, molecular weight, concentration, degree of hydrolysis, brine salinity, and reservoir temperature [1,2,4,6-10,12,13,16,17,20,23,30,31,34,35].

Adsorption increment was first explained by Martin [1]: an increment in the Total Dissolved Solids (TDS) results in a decrease of the hydrodynamic size of polymer molecule, thus decreasing electrostatic repulsion between the substrate and the polymer. As a result, adsorption increases.

NaCl and  $CaCl_2$  concentration varied in prepared brines in order to determine the effect of salinity on adsorption; an isotherm series were build based on these data in order to observe this phenomenon. Kaolinite, a commercial polymer (HPAM) and the salts mentioned above were used for the conduction of electrostatic testing.

Experimental testing was conducted at *NaCl* concentrations of 0,5; 1 and 2 wt%, in absence of any other salt, as it has been reported by Martin [1]; then, concentrations of  $CaCl_2$  of 2, 5 and 10 wt%, also in absence of other salts, were used as reported by Chiappa [2]. For each salinity values, solutions of 100, 200, 300, 400, 500, 600, 700, 800, 900 and 1.000 ppm of polymer were prepared, as reported by Green & Willhite [3] and Zheng [4], for the construction of the isotherms.

In order to ensure data reliability, a duplicate of each polymer concentration was prepared in order to guarantee a reliable tendency for experimental purposes. Triplicates were prepared for those cases where a clear tendency was not observed, given the stochastic nature of this type of testing.

#### 3. Experimental section

Screens of 50 and 200 mesh, a simple divider, a glass funnel, and a scale were used for the conduction of the testing procedure.

#### 3.1. Procedure

- Disintegration of substrate, drying of material in an oven, and straining of the mixture through 50 and 200 mesh screens in order to ensure a range of particle size.
- The simple is separated and a representative simple is taken; 5 g of sample and 15 g of polymeric solution of *NaCl* and *CaCl*<sub>2</sub>. at the corresponding concentration values are taken.
- The samples are placed in a container and this recipient is closed. Then, the samples are taken to an oven at reservoir temperature for two days. In this case, the value taken was the characteristic temperature of an oil field located in the Middle Magdalena Valley basin (VMM) in Colombia, that is, 60°C.
- Finally, the liquid is separated from the kaolinite aggregate by using a centrifuge or a qualitative paper filter in order to measure the concentration of polymer in the supernatant liquid.
- Measurements of the polymeric solution equivalent concentration was conducted with a spectrophotometer; the absorbance data are associated to the concentration data previously calibrated for each solution.

In order to control and validate this experimental testing stage, repeatability and reproducibility (r&R) of data were ensured. Repeatability is defined as the concordance of proximity between successive measurements of the same test under the same conditions. Reproducibility is the proximity among the results of successive experiments of the same set of tests when the measurement conditions change [5].

The whole set of tests was duplicated (repeatability) and finally, two more polymeric solutions were prepared: one with  $NaCl \ 1 \text{ wt\%}$  and the other with  $CaCl_2 \ 5 \text{ wt\%}$ . These solutions were diluted at the polymer concentration previously defined (from 100 to 1.000 ppm); the results for the NaCl and  $CaCl_2$  solutions are shown in the Figs. 1 and 2, respectively.



Figure 1. Repeatability and reproducibility (r&R) - polymer adsorption with NaCl 1 wt %. Source: The Authors.



Figure 2. Repeatability and reproducibility (r&R) - polymer adsorption with  $CaCl_2$  5 wt%. Source: The Authors.



Figure 3. Static adsorption for polymers with *CaCl*<sub>2</sub> brine. Source: The Authors.

Each mother solution was diluted at concentrations of 300, 500, 700 and 900 ppm, and new adsorption tests were conducted with these solutions in order to ensure their reproducibility.

The results of the adsorption tests with  $CaCl_2$  brines are shown in Fig. 3. A fast increment of the adsorption values is observed at low polymer concentration and stabilization is observed at the end of the curve; conversely, at low concentration of polymer, adsorption is practically independent from salinity and contrary to what has been reported for *NaCl* brines, the experiments based on *CaCl*<sub>2</sub> show a direct adsorption relation with regard to the concentration of polymer and salinity [8, 9, 23, 30, 31]. It is worth highlighting that no flocculation occurred in the experiments based on *CaCl*<sub>2</sub>. Contrary to the reports of Sheng [7], the adsorption tests with *NaCl* showed an inverse tendency: the higher salinity, the lower adsorption; this can be explained by the flocculation of kaolinite substrate; in the presence of *NaCl*, clays like kaolinite tend to flocculate thus decreasing the available area for adsorption. Meister [8] developed experiments with brines containing 5.600 ppm of sodium (*Na*), the adsorption value in this case was 417,5  $\mu$ g/g on kaolinite substrates while brines containing 1.900 ppm of sodium (*Na*) the result is 1.217  $\mu$ g/g due to substrate flocculation. This work presents *NaCl* concentrations in the brine of 0,5; 1 and 2 wt%, corresponding to 5.000, 10.000 and 20.000 ppm, respectively. Some authors suggest that flocculated kaolinite shows about 80% less than superficial area [9].

The Fig. 4 corresponds to the photographic record of this phenomenon and show the filters of flocculated samples and non-flocculated samples. In flocculated samples, the polymeric solution contained dispersed particles of kaolinite, while non-flocculated samples all kaolinite are decanted at the bottom of the container, and regardless the stirring conducted, the kaolinite remained agglomerate.



Figure 4. Photographic record of samples flocculation. Source: The Authors.



Figure 5. Static adsorption for polymers with *NaCl* brine. Source: The Authors.



Figure 6. Static adsorption with *NaCl* at 2 wt%. Source: The Authors.



Static Adsorption CaCl<sub>2</sub> - 2 wt%

• Duplicate • Original

Figure 7. Static adsorption with  $CaCl_2$  at 2 wt%. Source: The Authors.

It was proven that  $CaCl_2$  causes higher adsorption than *NaCl*: when conducting tests with same wt % of *NaCl* and *CaCl*<sub>2</sub> (2 wt% each, Fig. 6 and 7, respectively), the higher adsorption value with  $CaCl_2$  was 822 µg/g, compared to the value with *NaCl* (631 µg/g). Divalent ions increase adsorption in HPAM in greater proportion than monovalent ions as a result of an increased reduction of electrostatic repulsion between the substrate superficial charges and polymer molecules; this results in an increased affinity of the polymer for the brine [10], thus allowing increased polymer adsorption in the solid surface.

#### 4. Analytical models

The topic of adsorption has been extensively studied in the field of surface chemistry. Many analytical models have contributed to the quantification and prediction of this phenomenon being most of them based on experimental results. In this work, the models of Langmuir, Freundlich, and Henry were selected based on their satisfactory results for the determination of polymer adsorption.

Depending on each model, adsorption behavior varies depending on the adsorbent + adsorbate system so the experimental data were adjusted to the analytical model based on the minimum square regression operation and the MATLAB® tool.

#### 4.1. The Henry adsorption model

The Henry Model assumes that adsorption is directly proportional to solute concentration in a solution. However, one of the most limiting factors of this model is its strict application to low solute concentrations [19].

Batches ranging between 200 and 1.000 ppm [3] are applied during the polymer injection phase, and this range falls into the efficient values for the development of this work (maximum 400 ppm). Other factors assumed by this model, besides its application at low solute concentration are:

- Energy levels on the Surface are equivalent so there is not any preference of the adsorbate to occupy a specific place on the adsorbent.
- The surface is infinite. The reason for this assumption is based on the fact that the solute concentration is so low that if we compare it to the available adsorbent surface, the adsorbate can be retained with no restriction.
- There is no interaction between molecules once they are adsorbed.
- The type of adsorption occurring is a monolayer adsorption due to the low concentration of solute utilized.

The eq. (1) corresponds to the mathematical expression proposed by Henry to quantify adsorption based on solute concentration:

$$\widehat{C}\iota = K_H * Ci \tag{1}$$

Where  $\hat{C}i$  = adsorption,  $K_H$  = Henry's constant that depends on the adsorbate + adsorbent system, and Ci = solute concentration.

#### 4.2. The Langmuir adsorption model

Irving Langmuir [14] contributed largely to the field of Surface Chemistry in his work about adsorption on solid surfaces where he proposes a model to predict gas adsorption according to the pressure system and under the following assumptions:

- The adsorbing gas molecules adsorb into an immobile state.
- The adsorbate organizes in the form of a monolayer on the surface of the adsorbent.
- There are no interactions between adsorbate molecules on adjacent sites
- The solid surface has a certain amount of positions for adsorption and each position is equivalent in terms of energy levels. Therefore, there is not any preference to occupy a specific place.

When the adsorbate is a solute, an expression involving solute concentration is required. The eq. (2) shows the mathematical expression proposed by Langmuir.

$$\widehat{C}\iota = \frac{a * K_L * Ci}{1 + K_L * Ci}$$
<sup>(2)</sup>

Where  $\widehat{C\iota}$  = adsorption of solute on the surface; Ci =concentration in equilibrium of solute; a = maximum adsorption capacity of the system; and  $K_L$  = Langmuir affinity constant, equivalent to the ratio between the adsorption constant  $K_A$  and desorption  $K_D$ .

### 4.3. The Freundlich adsorption model

The Langmuir isotherm represented a great advance in the field of Surface Chemistry. However, this model works with many assumptions that, most of the time, do not correspond to the real conditions. As a result, many works attempting to improve the representation of this phenomenon were presented after its publication.

Erwin Finlay-Freundlich [11] developed in 1918 an empirical equation to determine adsorption based on a series of a gas-solid experiments. The Freundlich adsorption model has the following assumptions.

- The adsorbent surface is heterogeneous from the thermodynamic standpoint. As a result, the adsorbate molecules will allocate according to their energy level.
- Adsorbed molecules can overlap one on top of the other, producing a multilayer adsorption type, depending on the energy levels available on the surface.
- There is not any interaction between adsorbed molecules.

The expression for the gas - solid system can be adapted for those cases where the adsorbate is a solute and the adsorbent is a solid, as it is shown in the eq. (3):

$$\widehat{C}\iota = K_F * Ci^{1/n} \tag{3}$$

Where  $\hat{C}i$  = solute adsorption on the surface; Ci = solute concentration in equilibrium; and the constants  $K_F$  and 1/n are determined by experimental testing.

The number of absorbed molecules is not stabilized as a result of the multilayer adsorption; the various energy levels



Figure 8. Graphic tendency of the analyzed models. Source: The Authors.

on the surface shall produce an increasing amount of overlapping adsorbed molecules. Therefore, Freundlich isotherm does not show the characteristic *plateau* of Langmuir although it does show an increasing tendency. The Fig. 8 shows a comparison among the tendencies for each model described.

#### 5. Results and discussion

The experimental data collected were entered in a MATLAB® program using minimum square regression and the second derivation criterion to find discrepancies between experimental data and the data obtained from each analytical model. Finally, the model that best adjusted to the experimental data was selected.

$$\sum_{i=1}^{n} [f(x_i) - y_i]^2 \tag{4}$$

The graphs corresponding to the MATLAB® data are shown below. The number shown beside the legend of each model corresponds to the sum of quadratic errors. The eq. (4) indicates the error between the analytical model (xi) and the experimental data yi.

The Henry adsorption model, due to its low-concentration restriction, shows the best adjustment when compared to the models analyzed. However, this model does not include all the domain evaluated at experimental level. This is the reason why the Freundlich model is the model that best adjusts to the adsorption data on kaolinite substrates with *NaCl* at 0,5; 1 and 2 wt%, with an error of 20,619 - 10,662 and 10,288%, respectively, as it is shown in the Figs. 9, 10 and 11.

The bibliography confirms this tendency [12], that is, high concentration values generate high adsorption rates. The adsorbent surface is not homogeneous in this model and, therefore, adsorbate molecules shall allocate in the places where adsorption is allowed by the surface free energy. In other words, the polymer is adsorbed on preferential areas over the kaolinite and, as a result, the solid substrate will not saturate completely. Therefore, the adsorption curve will not stabilize and shall maintain an increasing tendency.



Figure 9. Static adsorption adjustment with *NaCl* - 0,5 wt%. Source: The Authors.



◆Data ▲Langmuir: 14,991 ■Freundlich: 10,662 ●Henry: 0,174

Figure 10. Static adsorption adjustment with *NaCl* - 1 wt%. Source: The Authors.



Figure 11. Static adsorption adjustment with *NaCl* - 2 wt%. Source: The Authors.



Figure 12. Static adsorption adjustment with  $CaCl_2$  - 2 wt%. Source: The Authors.

Similar to the experiments with *NaCl*, the Henry adsorption model adjusts correctly, at low polymer concentration, in the tests with *CaCl*<sub>2</sub>. However, the adjustment of polymer adsorption on kaolinite with *CaCl*<sub>2</sub> at 2 and 10 wt% is better when applying the Langmuir adsorption model, showing errors of 9,248 and 16,176 respectively, as its shown in the Figs. 12 and 14. Adsorption stabilization is obtained despite the increasing equilibrium concentration. However, adsorption in the presence of *CaCl*<sub>2</sub> at 5 wt% shows a similar tendency as reported by Freundlich, with an error of 12,112% (Fig. 13).

Finally, the Table 1 shows the values of the constants obtained by MATLAB® for each analytical model. It is observed that in the presence of *NaCl*, the Langmuir affinity constant,  $K_L$ , tends to decrease. This tendency is also observed in the maximum adsorption capacity, a; this is consistent with the experimental data and confirms that the system has less adsorption capacity; by contrast, *NaCl* concentration increases kaolinite flocculation. The constants  $K_F$  and 1/n of the Freundlich model also show this tendency: the greater salinity, the lower the values of these constants. Regarding *CaCl*<sub>2</sub>, the behavior observed is different.



◆Data ▲Langmuir: 14,628 ■Freundlich: 12,112 ●Henry: 0,075

Figure 13. Static adsorption adjustment with  $CaCl_2$  - 5 wt%. Source: The Authors.



◆Data ▲Langmuir: 16,176 ■Freundlich: 19,235 ●Henry: 0,076

Figure 14. Static adsorption adjustment with  $CaCl_2 - 10$  wt%. Source: The Authors.

Table 1. Constant table for each model

Analytical Models	Langmuir			Freundlich			Henry	
Constants	a [µg/g]	$K_L[L/mg]$	Error <sub>L</sub> [%]	1/n [ad]	$\left[\frac{K_{\rm F}}{\frac{mL}{g_{rock}}}\right]$	Error <sub>F</sub> [%]	$\left[\frac{K_H}{mL}\right]$	Error <sub>H</sub> [%]
Polymer NaCl 0,5 wt%	2.120,4	0,046	27,05	0,3507	311,22	20,61	5	15,670
Polymer NaCl 1 wt%	1.026,1	0,009	14,99	0,3125	119,68	10,66	2	0,174
Polymer NaCl 2 wt%	658,9	0,009	14,86	0,2712	99,22	10,28	2	0,147
Polymer CaCl <sub>2</sub> 2 wt%	872,8	0,010	9,24	0,3188	100,48	12,49	2	0,070
Polymer CaCl <sub>2</sub> 5 wt%	1.483,1	0,004	14,62	0,5036	43,71	12,11	2	0,075
Polymer CaCl <sub>2</sub> 10 wt%	2.059,1	0,004	16,17	0,5271	54,15	19,23	2	0,076

Source: The Author.

When the salt concentration increases, the Langmuir affinity constant tends to decrease while its maximum adsorption capacity increases. As it has been experimentally demonstrated, high  $CaCl_2$  concentrations represent high adsorption values and, therefore, a higher maximum adsorption capacity. The Freundlich constant 1/n increases as  $CaCl_2$  concentration increases; the  $K_F$  constant shows an abnormal behavior because it initially decreases and then increases.

Since the Henry adsorption model shows domain restriction at low concentration (up to 400 ppm), adsorption increases in a ratio 2:1 in all cases with regard to the concentration values, except when the polymer was in the presence of *NaCl* at 0.5 wt% where this ratio was 5:1. The assumptions of the Langmuir model are: the monolayer adsorption type occurring, lack of interaction between molecules, and lack of preference for a specific place on the substrate. This results in the occupation of the whole surface in theory as the polymer increases its concentration. This is demonstrated by the curve stabilization at the highest values of adsorbate concentration.

#### 6. Conclusions

An abnormal tendency was observed in the kaolinite substrates and *NaCl* polymeric solutions: high salinity values result in lower adsorption values due to flocculation of the kaolinite substrate. This process is inherent to the clay behavior.

The Langmuir adsorption model was the best adjusted to the experiments with  $CaCl_2$  due to its tendency to final stabilization. This can be attributed to the monolayer-type adsorption and the lack of interaction between adsorbed molecules. These two assumptions were considered by this model.

Regarding the data obtained with *NaCl*, it was observed that the Freundlich model shows greater affinity to the experimental tendency. This model establishes that the adsorbate will be allocated on preferential zones of the adsorbent and, therefore, the solid substrate will not be saturated resulting in the lack of stabilization in this curve.

The Freundlich adsorption model has some assumptions that could be more precise regarding the heterogeneity of

rock properties in a reservoir. However, the experiments with  $CaCl_2$  reveal that the Langmuir model was the best adjusted with NaCl.

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