

PRESSURE AND PRESSURE DERIVATIVE ANALYSIS FOR LONG NATURALLY FRACTURED RESERVOIRS USING THE *TDS* TECHNIQUE

ANÁLISIS DE PRESIÓN Y DERIVADA DE PRESIÓN EN YACIMIENTOS NATURALMENTE FRACTURADOS ALARGADOS USANDO LA TÉCNICA *TDS*

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ABSTRACT: Normally, in a heterogeneous formation, the transition period of flow from fissures to matrix takes place during the radial flow regime. However, depending upon the value of the interporosity flow parameter, this transition period can show up before or after the radial flow regime. An accurate understanding of how the reservoir produces and the magnitude of producible reserves can lead to competent decisions and adequate reservoir management.

So far, no methodology for interpretation of pressure tests under the above mentioned conditions has been presented. Currently, an interpretation study can only be achieved by non-linear regression analysis (simulation) which is obviously related to nonunique solutions. Therefore, in this paper, a detailed analysis of pressure and pressure derivative behavior for a vertical well in an elongated closed heterogeneous formation is presented. We studied independently each flow regime, especially the dual-linear flow regime since it is the most characteristic “fingerprint” of these systems; new equations to characterize such reservoirs is introduced and were successfully verified by interpreting both field and synthetic pressure tests for oil reservoirs.

KEY WORDS: Dual-linear flow regime, radial flow regime, interporosity flow parameter, dimensionless storativity coefficient

RESUMEN: Normalmente, en una formación heterogénea, el periodo de transición del flujo fracturas-matriz toma lugar durante el flujo radial. Sin embargo, dependiendo del valor del parámetro de flujo interporoso, dicha transición puede ocurrir antes o después del flujo radial. Un entendimiento preciso de la forma como el yacimiento produce y la magnitud de las reservas producibles puede conducir a una toma de decisión competente y una adecuada administración del yacimiento.

Hasta ahora, no existe metodología para interpretar pruebas de presión bajo las condiciones mencionadas anteriormente, por lo que el único estudio de interpretación debía conducirse usando análisis de regresión no lineal (simulación) que está relacionado con más de una solución. Por ende, en este artículo se presenta un análisis detallado de la presión y la derivada de presión para un pozo vertical que produce de una formación alargada y heterogénea. Se estudiaron independientemente los regímenes de flujo especialmente el flujo dual lineal puesto que reviste la “huella dactilar” más importante para estos sistemas. Se desarrollaron nuevas ecuaciones para caracterizar tales yacimientos, las cuales fueron satisfactoriamente verificadas con datos simulados y de campo.

PALABRAS CLAVE: Régimen de flujo dual lineal, régimen flujo radial, parámetro de flujo interporoso, coeficiente de almacenaje adimensional

1. INTRODUCTION

An important number of pressure tests are conducted in long and narrow reservoirs. This type of geometry, caused by fluvial deposition, faulting or deep sea fans deposition requires its proper identification and characterization.

Among the investigations on pressure tests for elongated systems during this decade, [1] introduced the application of the *TDS* technique for characterization of long and homogeneous reservoirs presenting new equations for estimation of reservoir area, reservoir width and geometric skin factors. In reference [2] introduced a new flow regime exhibiting a negative half slope on the pressure derivative curve once dual-linear flow has ended. They called this as parabolic flow. Reference [3] has also found this same behavior. However, they called it “dipolar flow”. Later, [4] studied the impact of the geometric skin factors on elongated systems. Characterization of pressure tests in elongated systems using the conventional method was presented by [5]. Also, reference [7] provided a way to estimate reservoir anisotropy when reservoir width is known in the mentioned systems from the combination of information obtained from the linear and radial flow regimes.

In the normal case for a heterogeneous formation, as consider by the double porosity model, the fluid flows from the fracture network to the well. Upon depletion, the fissures are fed by fluid from the matrix. This transition period is identified by a deflection of the pressure derivative curve and possesses a characteristic “V” shape. In many cases the transition period occurs during radial flow. In other words, the radial flow is interrupted by the transition period.

However, there are cases where the transition period occurs before or after the radial flow regime. For instance, [8] pointed out the occurrence of the transition period during

bilinear and linear flow regime periods in naturally fracture formations intercepted by a hydraulically fractured well. For these cases, the interporosity flow parameter, λ , is higher than 1×10^{-3} . In other cases, like the one dealt in this paper for elongated systems, the transition period occurs during the dual-linear flow regime, of course, later than the radial-flow regime. A modern technique known as the Tiab’s Direct Synthesis technique (*TDS* technique), [9] employs the log-log plot of pressure and pressure derivative curves to interpret pressure buildup and drawdown tests without using type-curve matching by using analytical equations derived for specific “fingerprints” found on the mentioned plot. Because of its simplicity and practicality, this technique is becoming more popular, and therefore, has been extended here to analyze pressure behavior in channelized heterogeneous oil formations.

2. SIMULATION RUNS

Fig. 1 illustrates the unique features for a long heterogeneous reservoir drained by a centered well in the reservoir. Table 1 contains the input data used for the simulations. It is first observed in this plot the occurrence of the radial flow regime. Then, the dual-linear flow shows up but it is interrupted by the transition period when fissures are fed by flux from the matrix. Finally, the late pseudosteady state flow regime is developed.

The other scenario considers the well off-centered inside the reservoir. Two possibilities can be presented, though. For the first one, the transition occurs before the single-linear flow, see Fig. 4. It implies that the chronological appearance of flow regimes is: radial, dual linear, transition period, single linear and pseudosteady state. The second one involves the interruption of the single-linear period by the transition period as depicted in Fig. 6. The chronological occurrence of the flow regimes

$$\lambda \propto t_w^2 \frac{k_m}{k_f} \tag{3.b}$$

3.1 Dual-linear flow regimes

All the characteristic points and lines are shown in Fig. 1 when the well is centered in the reservoir. For this case single-linear flow does not exist. After replacing Eqs. 2.b, 2.c and 2.e into Eq. 1.b, an expression to estimate reservoir width is obtained:

$$\sqrt{k_f} Y_E = \frac{4.064 qB}{h(t^* \Delta P')_{DL}} \sqrt{\frac{t_{DL} \mu}{\phi c_t \omega}} \tag{4.a}$$

If the pressure derivative, $(t^* \Delta P')_{DL}$ is read at the time, $t_{DL} = 1$ hr, Eq. 4.a becomes:

$$\sqrt{k_f} Y_E = \frac{4.064 qB}{h(t^* \Delta P')_{DL}} \sqrt{\frac{\mu}{\phi c_t \omega}} \tag{4.b}$$

The geometric skin factor caused by the convergence from radial to dual-linear flow regime is obtained by dividing Eq. 1.a by Eq. 1.b, and then, replacing the dimensionless parameters, Eqs. 2.a, 2.b, 2.c and 2.6,

$$S_{DL} = \left(\frac{\Delta P_{DL}}{(t^* \Delta P')_{DL}} - 2 \right) \frac{1}{19.601 Y_E} \sqrt{\frac{k_f t_{DL}}{\phi \mu c_t \omega}} \tag{5}$$

where ΔP_{DL} and $(t^* \Delta P')_{DL}$ are the pressure and pressure derivative points read at any arbitrary time during dual-linear flow regime, t_{DL} . ω can be obtained from any arbitrary point from the dual-linear flow regime on the pressure derivative curve. After plugging Eqs. 2.b, 2.c and 2. e into Eq. 1.b and solving for ω , it yields:

$$\omega = \frac{16.5186 \mu t_{DL}}{\phi c_t k_f} \left[\frac{qB}{Y_E h(t^* \Delta P')_{DL}} \right]^2 \tag{6}$$

3.2 Maximum point

The maximum point observed once the dual-linear flow vanishes is used for estimation of the interporosity flow parameter. It is observed in Fig. 2 that the pressure derivative always displays a unique maximum pressure derivative

value. Then, the following relationship is obtained:

$$\sqrt{\lambda} (t_D^* P_D')_{\max} = 0.000227 \tag{7}$$

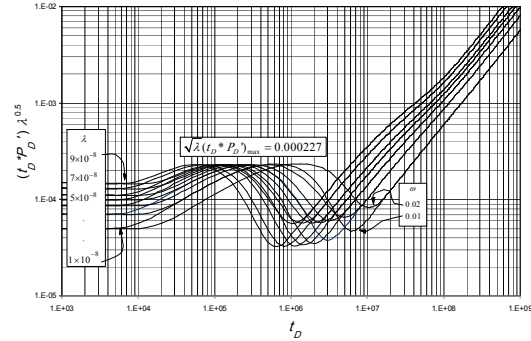


Figure 2. Dimensionless pressure derivative- $\lambda^{0.5}$ vs. dimensionless time for a long naturally fractured reservoir with different interporosity flow parameter values – Well centered in the reservoir

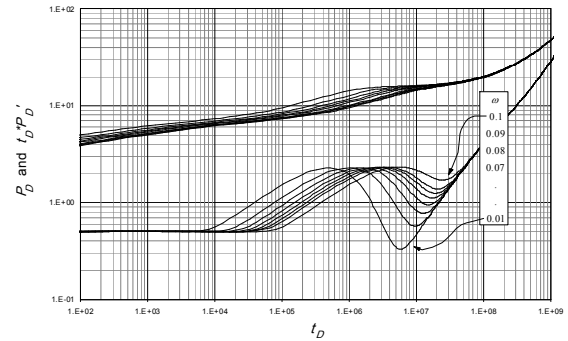


Figure 3. Effect of the dimensionless storativity coefficient, ω , on the pressure and pressure derivative for $\lambda = 2 \times 10^{-8}$ – Well centered in the reservoir

Replacing Eq. 2.b into Eq. 7, an approximation to estimate λ is given below:

$$\lambda = \left[\frac{0.0320524 q\mu B}{k_f h(t^* \Delta P')_{\max}} \right]^2 \tag{8}$$

3.3 Minimum point

Fig. 3 presents the pressure and pressure derivative behavior for different values of ω and $\lambda = 2 \times 10^{-8}$. We observe that ω is function of the minimum pressure derivative, the time at which this point takes place and the λ value. Then, we correlated these variables to obtain:

Correlation 1:

$$\omega = \frac{a + cx + e\lambda + gx^2 + i\lambda^2 + k\lambda x}{1 + bx + d\lambda + f\lambda^2 + h\lambda^2 + j\lambda x} \quad (9)$$

$$\begin{aligned} x &= (t_D * P_D')_{\min} \\ a &= -0.001453744345531936 \\ b &= -0.4034531139231534 \\ c &= 0.004969243560711644 \\ d &= 9384837.434697306 \\ e &= -25245.96831604798 \\ f &= 0.03947187690326912 \\ g &= -0.00884465599095826 \\ h &= -6557972683918.12 \\ i &= -371412686858.0194 \\ j &= -10246537.3284442 \\ k &= 2190827.21495808 \end{aligned}$$

This correlation is recommended since has an error of 0.12 %.

Correlation 2:

$$\begin{aligned} \omega &= a + b(t_D)_{\min} + c \ln x + d(t_D)_{\min}^2 + \\ &e \ln x^2 + f(t_D)_{\min} \ln x + g(t_D)_{\min}^3 + \\ &h \ln x^3 + i(t_D)_{\min} \ln x^2 + j(t_D)_{\min}^3 i \ln x \end{aligned} \quad (10)$$

$$\begin{aligned} x &= (t_D * P_D')_{\min} \\ a &= 0.311245913434052 \\ b &= -2.370850857204912 \times 10^{-8} \\ c &= 0.2991375371411262 \\ d &= -1.21694647249764 \times 10^{-15} \\ e &= 0.09804801848276096 \\ f &= 1.74956959326334 \times 10^{-8} \\ g &= 9.994911652511862 \times 10^{-23} \\ h &= 0.01139557746643557 \\ i &= 1.299349660522994 \times 10^{-8} \\ j &= -2.525663039488802 \times 10^{-15} \end{aligned}$$

This correlation has an error of 0.396 %.

3.4. Intersection points

The pressure derivative during late pseudosteady state flow regime is governed by:

$$(t_D * P_D')_{PSS} = 2\pi t_{DA} \quad (11)$$

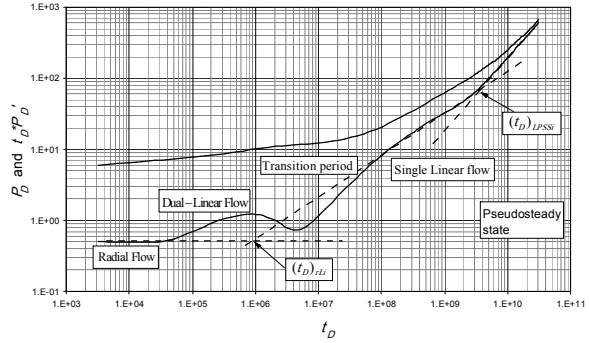


Figure 4. Dimensionless pressure and pressure derivative behavior for an elongated naturally fractured reservoir for $\omega = 0.05$, $\lambda = 1 \times 10^{-8}$ and $X_E = 29000$ ft – Well off-centered in the reservoir – Dual-linear flow is interrupted by the transition

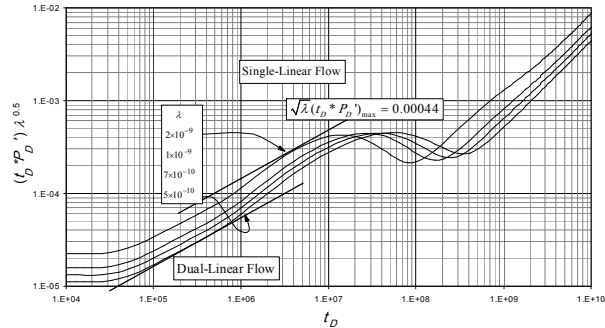


Figure 5. Dimensionless pressure derivative- $\lambda^{0.5}$ vs. dimensionless time for a naturally fractured reservoir with different interporosity flow parameter values and $\omega = 0.05$ – Well off-centered in the reservoir

The intersection of this line with the dual-linear flow regime pressure derivative line, Eq. 1.b, allows us to obtain an expression to estimate reservoir area once the dimensionless quantities are replaced:

$$A = 0.05829 \sqrt{\frac{Y_E^2 \omega k_f t_{DLPSS}}{\phi \mu c_i}} \quad (12)$$

The intercept of the radial flow line with the dual-linear flow line leads to confirm:

$$(t_D * P_D') = \frac{\sqrt{\pi t_D}}{W_D \sqrt{\omega}} = 0.5 \quad (13)$$

Replacing Eqs. 2.b, 2.c and 2.e in the above equations and solving for reservoir with, we obtain:

$$Y_E = 0.0575652 \sqrt{\frac{k t_{rDLi}}{\phi \mu c_i \omega}} \quad (14)$$

3.5. Early Pseudosteady State and Radial Flow Regime

Reference [9] presented the following relationship for the estimation of the wellbore storage coefficient,

$$C = \left(\frac{qB}{24} \right) \frac{t_i}{(t^* \Delta P')_i} = \left(\frac{qB}{24} \right) \frac{t_i}{\Delta P'_i} \quad (15)$$

Engler and Tiab (1996) presented the relationships for estimation of the permeability and mechanical skin factor as:

$$k_f = \frac{70.6 q \mu B}{h(t^* \Delta P')_r} \quad (16)$$

The mechanical skin factor is estimated from:

$$s_r = 0.5 \left(\frac{\Delta P'_r}{(t^* \Delta P')_r} - \ln \left(\frac{k_f t_r}{\omega \phi \mu c_i r_w^2} \right) + 7.43 \right) \quad (17)$$

Reference [1] also shown that the intercept between the radial flow and the pseudosteady state lines leads to an equation to estimate reservoir area:

$$A = \frac{k_f t_{rPSSi}}{301.77 \phi \mu c_i} \quad (18)$$

3.6 Linear-flow regime occurs after the transition period

Before the transition period the reservoir behaves as homogeneous; then, it appears the single-linear flow regime which governing equations for pressure and pressure derivative presented by reference [1]:

$$P_D = \frac{2\pi \sqrt{t_D}}{W_D} + S_L \quad (19.a)$$

$$(t_D * P_D)_L = \frac{\pi \sqrt{t_D}}{W_D} \quad (19.b)$$

The intersection points of the different flow regime lines are shown in Fig. 5. The equations for reservoir width, reservoir area and linear flow skin factors are obtained in a similar way as for the dual-linear case:

$$\sqrt{k} Y_E = \frac{7.2034 qB}{h(t^* \Delta P')_L} \sqrt{\frac{t_L \mu}{\phi c_i}} \quad (20)$$

$$Y_E = 0.1020 \sqrt{\frac{k_f t_{RLi}}{\phi \mu c_i}} \quad (21)$$

$$A = \sqrt{\frac{k_f t_{LPSSi} Y_E^2}{948.047 \phi \mu c_i}} \quad (22)$$

$$s_L = \left(\frac{\Delta P'_L}{(t^* \Delta P')_L} - 2 \right) \frac{1}{34.743 Y_E} \sqrt{\frac{k t_L}{\phi \mu c_i}} \quad (23)$$

3.7 Linear-flow regime occurs before the transition period

This case, sketched in Fig. 6, has the following governing equations:

$$P_D = \frac{10\pi \sqrt{t_D}}{6 W_D \sqrt{\omega}} + s_L \quad (24.a)$$

$$(t_D * P_D)_L = \frac{5\pi \sqrt{t_D}}{6 W_D \sqrt{\omega}} \quad (25.b)$$

Following a procedure similar to that in section 3.1 the following equations are obtained:

$$\sqrt{k_f} Y_E = \frac{6qB}{h(t^* \Delta P')_L} \sqrt{\frac{t_L \mu}{\phi c_i \omega}} \quad (26)$$

$$s_L = \left(\frac{\Delta P'_L}{(t^* \Delta P')_L} - 2 \right) \frac{1}{23.522 Y_E} \sqrt{\frac{k_f t_L}{\phi \mu c_i \omega}} \quad (27)$$

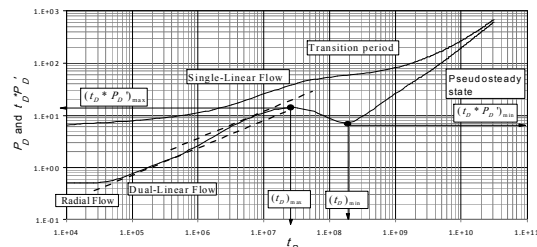


Figure 6. Dimensionless pressure and pressure derivative behavior for an elongated naturally fractured reservoir for $\omega = 0.05$, $\lambda = 1 \times 10^{-9}$ and $X_E = 29000$ ft – Well off-centered in the reservoir – Single-linear flow is interrupted by the transition

$$s_L = \frac{36\mu t_L}{\phi c_i k_f} \left(\frac{qB}{Y_E h(t^* \Delta P)_L} \right)^2 \quad (28)$$

$$Y_E = 0.08503 \sqrt{\frac{k_f t_{RLi}}{\phi \mu c_i \omega}} \quad (29)$$

$$A = \sqrt{\frac{k_f t_{LPPSi} \omega Y_E^2}{658.366 \phi \mu c_i}} \quad (30)$$

As shown in Fig. 6, the maximum point presented once the single-linear flow has been interrupted by the transition period results to be useful for the estimation the interporosity flow parameter. It is observed in Fig. 2 that the pressure derivative always displays a unique maximum pressure derivative value. Then, the following relationship is obtained:

$$\sqrt{\lambda} (t_D^* P_D')_{\max} = 0.00044 \quad (31)$$

Replacing Eq. 2.b into Eq. 31, an approximation to estimate λ is given below:

$$\lambda = \left[\frac{0.06213 q\mu B}{k_f h (t^* \Delta P)_{\max}} \right]^2 \quad (32)$$

For this case, there is a need of estimating ω from correlations. The following correlation has an error of 0.085 %.

$$\ln \omega = a + b\sqrt{\lambda} \ln \lambda + c\sqrt{\lambda} + d / \ln \lambda + ex + f\sqrt{x} \ln x + g\sqrt{x} + h \ln x + i / \sqrt{x} \quad (33)$$

$$\begin{aligned} x &= (t_D^* P_D')_{\min} \\ a &= -503.3662694927747 \\ b &= 67719.22178724448 \\ c &= 1023359.583295485 \\ d &= -2121.757955433415 \\ e &= 20.68488201371427 \\ f &= -121.8994586826316 \\ g &= 525.9038673208586 \\ h &= -229.1239182054168 \\ i &= -139.4598412994527 \end{aligned}$$

$$\begin{aligned} \omega &= a + b / (t_D)_{\min} + cx + d / (t_D)_{\min}^2 + ex^2 + fx / (t_D)_{\min} \\ &+ g / (t_D)_{\min}^3 + h x^3 + ix^2 / (t_D)_{\min}^2 + jx / (t_D)_{\min}^2 \end{aligned} \quad (34)$$

The former correlation has an error of 0.45 %.

$$\begin{aligned} x &= (t_D^* P_D')_{\min} \\ a &= 0.1837684859433586 \\ b &= -3609841.89782271 \\ c &= -0.03275900065412334 \\ d &= 4446584925703.334 \\ e &= -0.002829369841584908 \\ f &= -4327402.251581305 \\ g &= -1.993990486202685E+20 \\ h &= 0.000192725544328788 \\ i &= 1206668.159952826 \\ j &= 78159580419438.81 \end{aligned}$$

Needless to say that the total skin factor is estimated as the summation of the mechanical and geometric skin factors, such as:

$$s_t = s_r + s_{DL} + s_L \quad (35)$$

3.8. Unit-Slope Lines During the Transition Period

When the transition period takes place during the dual-linear flow regime, the fissures are fed by the matrix under pseudosteady state flow regime according to the model proposed in reference [10]. The expression governing this is given by:

$$\ln(t_D^* P_D')_{US} = a + b \ln t_{D,US} + c\sqrt{\lambda} \quad (36)$$

The former expression has a standard error of 0.707 % and a correlation coefficient of 0.99997 and should be used for dimensionless time values between 300000 and 3.69×10^7 . The coefficients are:

$$\begin{aligned} a &= -16.59119753322665 \\ b &= 0.9781590347464464 \\ c &= 3621.020392286202 \end{aligned}$$

As expressed by [11], during radial flow regime, the pressure derivative is governed by:

$$(t_D^* P_D')_{r1} = 0.5 \quad (37)$$

At the intersection point between the radial flow regime and the unit-slope line formed during the transition period an expression to estimate λ is obtained:

$$\lambda = \left\{ \frac{-0.69315 - a - b \ln t_{D,USi}}{c} \right\}^2 \quad (38)$$

When the transition occurs place after the single-linear flow regime is perfectly seen, the governing expression for the unit-slope transition line is also given by Eq. 36, which possesses a correlation coefficient of 0.99956 and should be used for dimensionless time values less than 4×10^7 . The coefficients are now:

$$\begin{aligned} a &= -17.25279260276791 \\ b &= 0.951844771427132 \\ c &= 23920.20465159351 \end{aligned}$$

4. STEP-BY-STEP PROCEDURES

4.1 Case 1 - transition occurs during the dual-linear flow period

Step 1 – Build a log-log plot of pressure and pressure derivative, identify and draw the early pseudosteady-state (if present), radial, dual-linear, single-linear (if exists) and late pseudosteady-state lines.

Step 2 - If the early-unit slope line exists, indicating wellbore storage, read any convenient point, t_i and either ΔP_i or $(t^* \Delta P)_i$, and find the wellbore storage coefficient with Eq. 15. Read the value of the pressure derivative during radial flow, $(t^* \Delta P)_r$, and calculate the bulk permeability using Eq. 16.

Step 3 – Find λ with Eq. 8 using the maximum point derivative during the transition period.

Step 4 – If the linear or single-linear flow regime is observed, read the pressure and pressure derivative values, ΔP_L and $(t^* \Delta P)_L$, at any convenient point on the linear flow regime, t_L , and find reservoir width, Y_E , using Eq. 20 and 21, and single-linear skin factor with Eq. 23. Otherwise estimate ω with correlations 9 and/or 10 using the coordinates of minimum point,

Step 5 – If the single-linear flow regime is observed, read the intercepts of this line with the radial flow, t_{rLi} and the pseudosteady state, t_{LPSSi} ,

lines. Find reservoir area with Eq. 22 and reservoir width with Eq. 21.

Step 6 - Read the pressure and pressure derivative values, ΔP_{DL} and $(t^* \Delta P)_{DL}$, at any convenient point on the dual-linear flow regime, t_{DL} , and find ω using Eq. 6. Alternatively, either Y_E or ω can be estimated with Eqs. 4.a or 14. Other values of ω may be estimated from the correlations given by Eqs. 9 and 10. For this purpose the coordinates of the minimum point, t_{min} and $(t^* \Delta P)_{min}$, during the transition period have to be used. An average value of ω may be obtained.

Step 7 - Find the geometric skin factor, s_{DL} using Eq. 5 and compute reservoir width using Eq. 14. Read the point of intersection of the radial and dual-linear flow lines, t_{rDLi} and re-estimate reservoir width with Eqs. 4.a and 14.

Step 8 – Read the intersection point between the late pseudosteady state line with the dual-linear, t_{DLPPSi} , and radial, t_{rPSSi} , lines. Calculate reservoir area with Eqs. 12 and 18.

Step 9 – Read the intersection point between the pseudosteady state transition line with the radial line, t_{USi} , and estimate the interporosity flow parameter with Eq. 38.

Step 10 – Estimate the total skin factor with Eq. 35.

4.2 Case 2 - linear-flow regime occurs before the transition period

Step 1 – 2 – Same as case 1.

Step 3 – Find λ with Eq. 8 using the maximum point derivative during the transition period.

Step 4 – Estimate ω with correlations 33 and 34. Read the pressure and pressure derivative values, ΔP_L and $(t^* \Delta P)_L$, at any convenient point on the linear flow regime, t_L , and find ω from Eq. 28. This new value may be averaged with the value obtained from the dual-linear flow. Then, find reservoir width, Y_E , using Eq. 26, and single-linear skin factor with Eq. 27.

Step 5 – Read the intercepts of this line with the radial flow, t_{rLi} and the pseudosteady state, t_{LPSSi} , lines. Find reservoir area with Eq. 29 and reservoir width with Eq. 30.

Step 6 - Read the pressure and pressure derivative values, ΔP_{DL} and $(t^*\Delta P)_{DL}$, at any convenient point on the dual-linear flow regime, t_{DL} , and find ω using Eq. 6. Alternatively, either Y_E or ω can be estimated with Eqs. 4.a or 14.

Step 7 - Find the geometric skin factor, s_{DL} using Eq. 5 and compute reservoir width using Eq. 14. Read the point of intersection of the radial and dual-linear flow lines, t_{rDLi} , and re-estimate reservoir width with Eqs. 4.a and 14.

Step 8 – Read the points of intersection of the single-linear flow line with the radial flow, t_{rLi} and the pseudosteady state, t_{LPSSi} , lines. Find reservoir width using Eq. 29 and reservoir area with Eq. 30.

Step 9 – 10 - Same as steps 9 and 10 of case 1.

5. EXAMPLES

5.1 Synthetic example 1

The log-log plot of pressure and pressure derivative for an example generated with information from table 1 is given in Fig. 7. Characterize this hypothetic reservoir using the methodology presented here.

Solution

From Fig. 7, the following data were read:

$$\begin{aligned} (t^*\Delta P)_r &= 25.556 \text{ psi} & \Delta P_r &= 337.556 \text{ psi} \\ t_r &= 0.2 \text{ hr} & t_{rDLi} &= 1.85 \text{ hr} \\ (t^*\Delta P)_{DL} &= 33.386 \text{ psi} & \Delta P_{DL} &= 411.1960 \text{ psi} \\ t_{DL} &= 3.177 \text{ hr} & t_{DLPSi} &= 20000 \text{ hr} \\ (t^*\Delta P)_{max} &= 76.66 \text{ psi} & t_{rPSSi} &= 195 \text{ hr} \\ t_{USi} &= 175 \text{ hr} \end{aligned}$$

Permeability is estimated from Eq. 16:

$$k = \frac{70.6 q\mu B}{h(t^*\Delta P)_r} = \frac{70.6 * 300 * 1.26 * 1.2}{50 * 25.556} = 25.061 \text{ md}$$

The dimensionless storativity coefficient is estimated with Eq. 6,

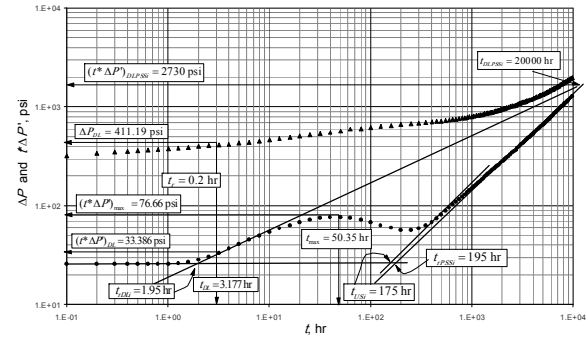


Figure 7. Pressure and pressure derivative plot for synthetic example 1

$$\omega = \frac{16.5186 * 1.26 * 3.177}{0.15 * 3 \times 10^{-6} * 25.061} \left[\frac{300 * 1.2}{1800 * 50 * 33.386} \right]^2$$

$$\omega = 0.085$$

Reservoir width is estimated from the intersection of the radial line with the dual-linear line, using Eq. 14,

$$Y_E = 0.0575652 \sqrt{\frac{25.061 * 1.85}{0.15 * 1.26 * 3 \times 10^{-6} * 0.08417}}$$

$$Y_E = 1794.21 \text{ ft}$$

Reservoir drainage area is estimated with Eqs. 12 and 18,

$$A = 0.05828558 \sqrt{\frac{1800^2 * 0.08417 * 25.061 * 20000}{0.15 * 1.26 * 3 \times 10^{-6}}}$$

$$A = 28618578 \text{ ft}^2$$

$$A = \frac{k t_{rPSSi}}{301.77 \phi \mu c_i}$$

$$A = \frac{25.061 * 195}{301.77 * 0.15 * 1.26 * 3 \times 10^{-6}}$$

$$A = 28561031.4 \text{ ft}^2$$

The interporosity flow parameter, λ , is approximated with Eq. 8, so that:

$$\lambda = \left[\frac{0.0320524 * 300 * 1.26 * 1.2}{25.061 * 50 * 76.6619682} \right]^2 = 2.295 \times 10^{-8}$$

Permeability is verified from Eq. 4.b (Note: Reservoir width may be verified instead):

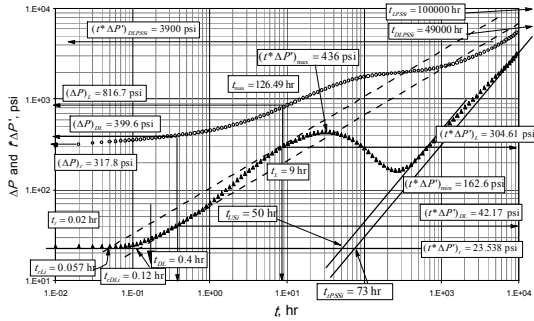


Figure 8. Pressure and pressure derivative plot for synthetic example 2

$$k = \left[\frac{4.06416 * 300 * 1.2}{1800 * 50 * 33.386} \sqrt{\frac{3.177 * 1.26}{0.15 * 3 \times 10^{-6} * 0.08417}} \right]^2$$

$$k = 25.06 \text{ md}$$

The dimensionless time at the point of intercept between the radial-flow line and unit-slope transition line is determined with Eq. 2.c as:

$$t_{D,USi} = \frac{0.0002637 * 175}{0.15 * 1.26 * 3 \times 10^{-6} * 0.35^2} = 16609977.32$$

The interporosity flow parameter can be estimated from Eq. 38,

$$\lambda = \left\{ \frac{0.69315 + 16.5912 - 0.97816 \ln(16609977.32)}{3621.0204} \right\}$$

$$\lambda = 1.013 \times 10^{-8}$$

The mechanical, geometric and total skin factors are calculated with Eqs. 17, 5 and 35, respectively,

$$s_r = 0.5 \left(\frac{337.8}{25.56} - \ln \left(\frac{25.06 * 0.2}{0.15 * 1.26 * 3 \times 10^{-6} * 0.35^2 * 0.084} \right) + 7.43 \right)$$

$$s_r = 0.04$$

$$s_{DL} = \left(\frac{441.2}{33.39} - 2 \right) \frac{1}{34.74 * 1800} \sqrt{\frac{25.06 * 3.18}{0.15 * 1.26 * 3 \times 10^{-6} * 0.085}}$$

$$s_{DL} = 6.74$$

$$s = s_r + s_{DL} = 0.04 + 6.74 = 6.78$$

From this example we can affirm that the proposed equations are correct since the simulated data agree quite well with the results of this exercise.

4.2 Synthetic example 2

A synthetic pressure test for a well off-centered in a reservoir was also generated with information from table 1. The pressure and pressure derivative plot is provided in Fig. 8. It is required to estimate permeability, skin factors, reservoir width and area and the naturally fractured reservoir parameters.

Solution

From Fig. 8, the following data were read:

- $(t^* \Delta P')_r = 23.538 \text{ psi}$ $\Delta P_r = 317.8 \text{ psi}$
- $t_r = 0.1 \text{ hr}$ $t_{rDLi} = 0.12 \text{ hr}$
- $(t^* \Delta P')_{DL} = 42.17 \text{ psi}$ $\Delta P_{DL} = 399.6 \text{ psi}$
- $t_{DL} = 0.4 \text{ hr}$ $t_{DLPSSi} = 43000 \text{ hr}$
- $(t^* \Delta P')_{max} = 436 \text{ psi}$ $t_L = 9 \text{ hr}$
- $(t^* \Delta P')_L = 304.61 \text{ psi}$ $\Delta P_L = 816.7 \text{ psi}$
- $t_{rPSSi} = 73 \text{ hr}$ $(t^* \Delta P')_{min} = 162.7 \text{ psi}$
- $t_{rLi} = 0.057 \text{ hr}$ $t_{LPSSi} = 100000 \text{ hr}$
- $t_{US,i} = 50 \text{ hr}$

All the computations are summarized as follows:

Parameter	Value	Eq. used
k , md	50	16
λ	2.25×10^{-9}	32
λ	3.14×10^{-9}	38
$(t_D^* P_D')_{min}$	3.46	2.b
$(t_D)_{min}$	13.9×10^6	2.c
ω	0.03	34
Y_{E_s} , ft	1511.5	14
Y_{E_s} , ft	1513.1	29
Y_{E_s} , ft	1540.2	4.a
Y_{E_s} , ft	1468.2	26
ω	0.03	6
ω	0.029	28
A_1 , ft ²	40.3×10^6	18
A_1 , ft ²	39.9×10^6	12
A_1 , ft ²	41.3×10^6	30
s_r	-0.02	17
s_{DL}	12.2	5
s_L	4.32	27
s_t	16.5	35

4.3 Field example

This example was taken from a pressure test run in a South American well. Reservoir, fluid and well parameters are provided in table 1 and the pressure and pressure derivative plot is provided in Fig. 9. A reservoir permeability of 2700 md was obtained from a previous test. Find reservoir width, reservoir area, skin factor, interporosity flow parameter and the dimensionless storativity coefficient.

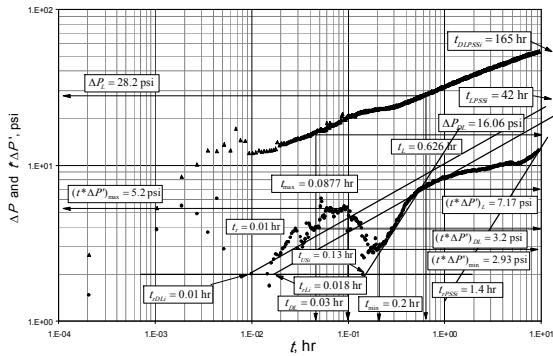


Figure 9. Pressure and pressure derivative plot for field case example

Solution

The dual-linear flow is very noisy. The following data were read from Fig. 9,

$$\begin{aligned} (t^* \Delta P)_r &= 1.99 \text{ psi} & \Delta P_r &= 11.98 \text{ psi} \\ t_r &= 0.01 \text{ hr} & t_{rDLi} &= 0.01 \text{ hr} \\ (t^* \Delta P)_{DL} &= 3.2 \text{ psi} & \Delta P_{DL} &= 16.06 \text{ psi} \\ t_{DL} &= 0.03 \text{ hr} & (t^* \Delta P)_{max} &= 5.2 \text{ psi} \\ \Delta P_L &= 28.2 \text{ psi} & t_L &= 0.626 \text{ hr} \\ (t^* \Delta P)_L &= 7.17 \text{ psi} & t_{rDLi} &= 0.018 \text{ hr} \\ (t^* \Delta P)_{min} &= 2.93 \text{ psi} & t_{min} &= 0.2 \text{ psi} \\ t_{DLPSi} &= 165 \text{ hr} & t_{LPSi} &= 42 \text{ hr} \\ t_{rPSi} &= 1.4 \text{ hr} & t_{USi} &= 0.13 \text{ hr} \\ t_{max} &= 0.0877 \text{ psi} \end{aligned}$$

The minimum dimensionless parameters are estimated from Eq. 2.b and 2.c:

$$t_D * P_D' = \frac{k_r h (t^* \Delta P)}{141.2 q \mu B} = \frac{2700 * 84 * 2.93}{141.2 * 457 * 9.4 * 1.48} = 0.74$$

$$t_D = \frac{0.0002637 kt}{\phi \mu (c_t)_{f+m} r_w^2}$$

$$t_D = \frac{0.0002637 * 2700 * 0.2}{0.0734 * 9.4 * 9.899 \times 10^{-6} * 0.5^2} = 92768.12$$

Using these dimensionless values in correlation 9, $\omega = 0.056$. The reservoir width is estimated with Eq. 20,

$$Y_E = \frac{7.2034 * 457 * 1.49}{\sqrt{2700 * 84 * 7.17}} \sqrt{\frac{0.627 * 9.4}{0.0734 * 9.9 \times 10^{-6}}} = 446.4 \text{ ft}$$

ω is estimated with Eq. 4.a, 6 and 14,

$$\omega = \frac{16.5186 * 9.4 * 0.03}{0.0734 * 2700 * 9.9 \times 10^{-6}} \left[\frac{457 * 1.5}{441.4 * 84 * 3.2} \right]^2 = 0.078$$

$$\omega = \frac{4.064 * 457 * 1.5}{\sqrt{2700 * 84 * 3.2}} \sqrt{\frac{0.03 * 9.4}{0.0734 * 9.9 \times 10^{-6}}} = 0.0782$$

$$\omega = \left(\frac{0.05756}{441.4} \right)^2 \frac{2700 * 0.01}{0.0734 * 9.4 * 9.899 \times 10^{-6}} = 0.068$$

The value of ω from correlation 9 is close to the ones found from the analytical equations. The interporosity flow parameter, λ , is approximated with Eq. 8, so that:

$$\lambda = \left(\frac{0.03205 * 457 * 9.4 * 1.5}{2700 * 84 * 5.2} \right) = 3.8 \times 10^{-8}$$

The dimensionless time at the point of intercept between the radial-flow line and unit-slope transition line is determined with Eq. 2.c as:

$$t_{D,USi} = \frac{0.0002637 * 0.13}{0.0734 * 9.4 * 9.899 \times 10^{-6} * 0.5^2} = 54207.83$$

Eq. 38 should not be used since the dimensionless time is less than 500000. Reservoir area is estimated by Eqs. 12, 18 and 22, as follows:

$$A = 0.05829 \sqrt{\frac{441.4^2 * 0.078 * 2700 * 165}{0.0734 * 9.4 * 9.899 \times 10^{-6}}}$$

$$A = 1835227.6 \text{ ft}^2$$

$$A = \frac{2700 * 1.4}{301.77 * 0.0734 * 9.4 * 9.899 \times 10^{-6}}$$

$$A = 1834004.93 \text{ ft}^2$$

$$A = \sqrt{\frac{2700 * 42 * 441.4^2}{948.047 * 0.0734 * 9.4 * 9.899 \times 10^{-6}}}$$

$$A = 1847210.2 \text{ ft}^2$$

The skin factors are estimated with Eqs. 17, 5, 23 and 35, respectively,

$$s_r = 0.5 \left[\frac{11.98}{1.99} - \ln \left(\frac{2700 * 0.01}{0.0734 * 9.4 * 9.899 \times 10^{-6} * 0.5^2 * 0.078} \right) + 7.43 \right]$$

$$s_r = -2.84$$

$$s_{DL} = \left(\frac{16.06}{3.2} - 2 \right) \frac{1}{19.601 * 441.4}$$

$$\sqrt{\frac{2700 * 0.03}{0.0734 * 9.4 * 9.899 \times 10^{-6} * 0.078}} = 8.6$$

$$s_L = \left(\frac{28.2}{7.17} - 2 \right) \frac{1}{34.743 * 441.6}$$

$$\sqrt{\frac{2700 * 0.626}{0.0734 * 9.4 * 9.899 \times 10^{-6}}} = 3.96$$

$$s_t = s_r + s_{DL} + s_L = -2.84 + 8.6 + 3.96 = 9.7$$

5. COMMENTS ON THE RESULTS

The synthetic examples are shown to verify the proposed equations. A good agreement is observed between the input data with the resulted values. Needless to say the several of the parameters are obtained from more than one source giving more strength to the results. The naturally fractured parameters, λ and ω , are very sensitive. It is customary accepted to have one order of magnitude in error for the interporosity flow parameter when comparing to other methods, and even with the same *TDS* technique. However, for this case the results are very close.

6. CONCLUSION

New equations for interpretation of pressure and pressure derivative data are introduced for naturally fractured formations when the transition period due to the depletion in the fissures occurs during either dual-linear or single-linear flow regimes. Also, correlations for

estimation the interporosity flow parameter was introduced when the dual-linear flow is interrupted by the mentioned transition. The validity of the equations was carried out by successfully comparing with simulated results.

7. RECOMMENDATIONS

This work can be extended for the case when the transition period occurs during the late pseudosteady state flow regime which may be present when dealing with rate transient analysis. We also recommend correlating the minimum to obtain expressions similar to Eqs. 9 and 10. Also, the governing equation for the pseudosteady state flow during the transition may be generated so more equations to determine the naturally fracture reservoir parameters can be introduced.

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NOMENCLATURE

A	Area, ft ²
B	Oil formation factor, rb/STB
c_t	Compressibility, 1/psi
F_M	Correction factor to account for the
h	Formation thickness, ft
K	Permeability, md
P	Pressure, psi
P_D'	Dimensionless pressure derivative
P_D	Dimensionless pressure
P_i	Initial reservoir pressure, psi
P_{wf}	Well flowing pressure, psi
q	Flow rate, bbl/D. For gas reservoirs
r_D	Dimensionless radius
r_e	Drainage radius, ft
r_w	Well radius, ft

s	Skin factor
s_i	Total skin factor
t	Time, hr
$t^*\Delta m(P)$	Pseudopressure derivative function,
t_D	Dimensionless time

Greek

Δ	Change, drop
Δt	Flow time, hr
ϕ	Porosity, fraction
μ	Viscosity, cp
λ	Interporosity flow parameter
ω	Dimensionless storativity ratio

Suffices

D	Dimensionless
DA	Dimensionless referred to reservoir
DL	Dual-linear
DL	Dual-linear at 1 hr
$DLPS_i$	Intersection of dual-linear line with
f	Fracture network, fissures
$f+m$	Total system (fracture network +
i	Intersection or initial conditions
L	Single-linear
$LPSS_i$	Intersection of single-linear line with
m	Matrix
PSS	Pseudosteady
r	radial flow
$rPSS_i$	Intersection of pseudosteady-state line
rDL_i	Intersection of radial line with dual-
rL_i	Intersection of radial line with single-

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